

# Correlation constants for chemical compounds

Procedures to speed calculations for:

- Heat capacities
- Heats of formation
- Free energies of formation
- Heats of vaporization

Carl L. Yaws, Lamar University, and others\*

□ Correlation constants in an easy-to-use tabular format are especially applicable for rapid engineering usage with the hand calculator or computer. The constants are based on extensive documentation and scores of experimental data. Margins of statistical accuracy are noted for each chemical listed.

For gas-phase properties, extrapolation to lower (200 K) and higher (1,500 K) temperatures provides

reliable results. Extrapolation for liquid-phase properties is not required in most cases because the temperature range covers melting point to critical point.

The tabulated constants may be used in various activities associated with the chemical process industries, such as chemical-reaction engineering, thermodynamics, fluid flow, heat transfer, mass transfer and process design.

## HEAT CAPACITIES OF GAS

Robin W. Borreson, Gordon R. Schorr and Carl L. Yaws

The heat capacity of major chemicals is important for engineering design in the chemical process industries. For example, in gas-phase chemical reactions, heat capacities for the gas are required to determine the energy (heat) necessary to bring the chemical compound up to reaction temperature. Additional usage includes heat-exchanger and energy-balance design calculations. The heat capacity of mixtures may be determined from the heat capacities of the individual components contained in the mixtures.

### Correlation constants—Table 22—1

The correlation for heat capacity of the ideal gas at low pressure is a series expansion in temperature:

$$C_p^\circ = A + BT + CT^2 + DT^3 \quad (22-1)$$

where  $C_p^\circ$  = heat capacity of ideal gas at low pressure, cal/(g-mol)(°K);  $A$ ,  $B$ ,  $C$  and  $D$  = characteristic constants for the chemical compound; and  $T$  = temperature, °K.

The correlation constants ( $A$ ,  $B$ ,  $C$  and  $D$ ) were determined from a least-squares fit of the available data. The numerous data points were processed with a generalized least-squares computer program for minimizing the deviation.

A comparison of calculated and data values is shown in Fig. 22-1 for a representative chemical. In most cases, average deviations between correlation and data results are less than 0.5%.

*Example 22-1*—Let us estimate the heat capacity of

\*For author biographies, see p. 87.

Correlation constants: heat capacity of ideal gas

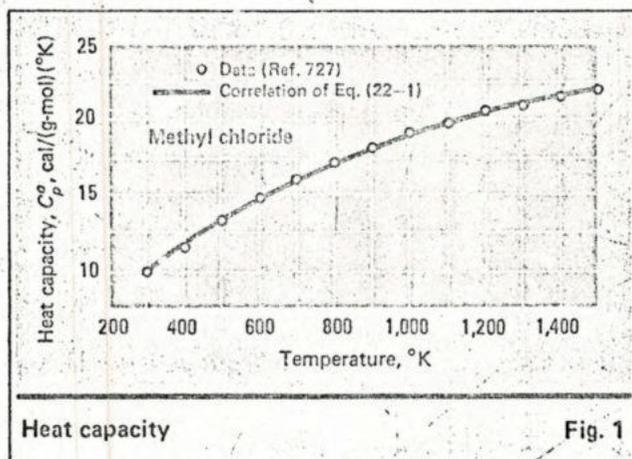
Table 22-1

Compound	$C_p^0 = A + BT + CT^2 + DT^3$				$C_p^0$ at 298 K, cal/(g-mol)(°K)	Range, °K	Average error, %	Data points, no.	References
	A	$B \times 10^3$	$C \times 10^6$	$D \times 10^9$					
<b>Halogens</b>									
Fluorine, F <sub>2</sub>	5.89	6.94	-5.48	1.52	7.51	298-1,500	0.225	59	7,15, 6,18,20
Chlorine, Cl <sub>2</sub>	7.00	5.05	-4.39	1.30	8.15	298-1,500	0.234	60	7,15, 6,18,20
Bromine, Br <sub>2</sub>	8.11	2.32	-2.04	0.62	8.64	298-1,500	0.131	60	7,15, 6,18,20
Iodine, I <sub>2</sub>	8.57	1.13	-0.91	0.27	8.83	298-1,500	0.059	51	7,15, 6,18,20
<b>Sulfur oxides</b>									
Sulfur dioxide, SO <sub>2</sub>	5.85	15.4	-11.1	2.91	9.52	298-1,500	0.33	46	7,15, 17, 546
Sulfur trioxide, SO <sub>3</sub>	3.96	34.6	-26.8	6.96	12.06	298-1,500	2.03	22	7,15
<b>Nitrogen oxides</b>									
Nitrous oxide, N <sub>2</sub> O	5.64	14.8	-9.68	2.33	9.25	298-1,500	0.142	13	7,15
Nitric oxide, NO	6.93	-0.065	2.23	-0.98	7.08	298-1,500	0.339	13	7,15
Nitrogen dioxide, NO <sub>2</sub>	5.53	13.2	-7.96	1.71	8.80	298-1,500	0.131	13	7,15
<b>Carbon oxides</b>									
Carbon monoxide, CO	6.92	-0.65	2.80	-1.14	6.94	298-1,500	0.244	21	7,15
Carbon dioxide, CO <sub>2</sub>	5.14	15.4	-9.94	2.42	8.91	298-1,500	0.155	21	7,15
<b>Hydrogen halides</b>									
Hydrogen fluoride, HF	7.16	-1.01	1.34	-0.28	6.96	298-1,500	0.093	39	7,11, 15, 34
Hydrogen chloride, HCl	7.24	-1.76	3.07	-1.00	6.96	298-1,500	0.066	47	7,11, 15, 34
Hydrogen bromide, HBr	7.15	-1.52	3.21	-1.13	6.95	298-1,500	0.132	26	7,15, 34
Hydrogen iodide, HI	6.95	-0.76	2.81	-1.09	6.94	298-1,500	0.223	26	7,15, 34
<b>Nitrogen hydrides</b>									
Ammonia, NH <sub>3</sub>	6.07	8.23	-0.16	-0.66	8.49	298-1,500	0.189	28	7,15
Hydrazine, N <sub>2</sub> H <sub>4</sub>	3.87	35.7	-23.0	5.98	12.63	298-1,500	1.17	47	7,15, 189, 218
<b>Hydrogen oxides</b>									
Water, H <sub>2</sub> O	8.10	-0.72	3.63	-1.16	8.18	298-1,500	0.438	79	7,15, 18, 646
Hydrogen peroxide, H <sub>2</sub> O <sub>2</sub>	5.52	19.8	-13.9	3.74	10.28	298-1,500	1.082	63	7,15, 18, 241, 245, 251
<b>Diatomic gases</b>									
Hydrogen, H <sub>2</sub>	6.88	-0.022	0.21	0.13	6.90	298-1,500	0.454	100	7,15, 16, 19, 646
Nitrogen, N <sub>2</sub>	7.07	-1.32	3.31	-1.26	6.94	298-1,500	0.167	100	7,15, 16, 19, 646
Oxygen, O <sub>2</sub>	6.22	2.71	-0.37	-0.22	6.99	298-1,500	0.28	100	7,15, 16, 19, 646
<b>Inert gases</b>									
Helium, He	4.97	-	-	-	4.97	298-1,500	-	-	16, 18
Neon, Ne	4.97	-	-	-	4.97	298-1,500	-	-	16, 18
Argon, Ar	4.97	-	-	-	4.97	298-1,500	-	-	16, 18
<b>Olefins</b>									
Ethylene, C <sub>2</sub> H <sub>4</sub>	0.934	36.9	-19.3	4.01	10.32	298-1,500	0.415	34	7,11, 15
Propylene, C <sub>3</sub> H <sub>6</sub>	0.68	56.8	-28.6	5.6	15.26	298-1,500	0.150	17	15, 637
1-Butene, C <sub>4</sub> H <sub>8</sub>	-0.515	83.1	-45.5	9.8	20.48	298-1,500	0.100	22	15, 646
<b>Alkanes</b>									
Methane, CH <sub>4</sub>	5.04	9.32	8.87	-5.37	8.53	298-1,500	1.635	37	15, 461, 646
Ethane, C <sub>2</sub> H <sub>6</sub>	2.46	36.1	-7.0	-0.46	12.57	298-1,500	1.010	44	15, 461, 646
Propane, C <sub>3</sub> H <sub>8</sub>	-0.58	69.9	-32.9	6.54	17.50	298-1,500	0.649	44	15, 461, 646
<b>Xylenes</b>									
<i>o</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-3.69	142.0	-82.1	19.2	31.85	298-1,500	0.108	22	15, 646
<i>m</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-6.67	149.0	-87.6	19.55	30.48	298-1,500	0.121	22	15, 646
<i>p</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-6.3	146.0	-84.4	18.6	30.32	298-1,500	0.136	32	15, 637, 646
<b>Aromatics</b>									
Benzene, C <sub>6</sub> H <sub>6</sub>	-8.79	116.0	-76.1	18.9	19.50	298-1,500	0.333	91	3, 15, 18, 19, 484
Naphthalene, C <sub>10</sub> H <sub>8</sub>	-13.02	185.0	-126.0	31.9	32.05	298-1,500	0.240	25	3, 15, 637
<b>Alkyl aromatics</b>									
Toluene, C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	-9.34	138.5	-87.2	20.6	24.73	298-1,500	0.505	21	15, 417
Ethylbenzene, C <sub>6</sub> H <sub>5</sub> C <sub>2</sub> H <sub>5</sub>	-8.42	159.0	-99.5	23.7	30.75	298-1,500	0.186	21	15, 417
Cumene, C <sub>6</sub> H <sub>5</sub> CH(CH <sub>3</sub> ) <sub>2</sub>	-9.38	165.7	-117.0	28.1	36.26	298-1,500	0.198	35	15, 417, 646
<b>Benzene derivatives</b>									
Chlorobenzene, C <sub>6</sub> H <sub>5</sub> Cl	-5.97	123.0	-88.9	24.1	23.43	298-1,000	0.137	10	15, 416
Aniline, C <sub>6</sub> H <sub>5</sub> NH <sub>2</sub>	-8.11	143.4	-107.0	30.7	25.93	298-1,000	0.149	10	15, 416
Phenol, C <sub>6</sub> H <sub>5</sub> OH	-5.68	126.0	-85.4	20.5	24.82	298-1,000	0.236	10	15, 416, 418
<b>Cycloalkanes</b>									
Cyclopropane, C <sub>3</sub> H <sub>6</sub>	-6.20	79.8	-50.5	12.2	13.36	298-1,000	0.197	18	5, 416, 637
Cyclobutane, C <sub>4</sub> H <sub>8</sub>	-9.0	105.0	-62.9	14.5	17.25	298-1,500	0.153	19	5, 416, 637
Cyclopentane, C <sub>5</sub> H <sub>10</sub>	-13.4	132.5	-76.09	16.8	19.82	298-1,500	0.206	24	15, 416, 646
Cyclohexane, C <sub>6</sub> H <sub>12</sub>	-16.2	165.0	-91.3	18.8	25.41	298-1,500	0.294	24	15, 416, 646
<b>Olefin monomers</b>									
Isobutylene, C <sub>4</sub> H <sub>8</sub>	1.22	79.5	-43.2	9.35	21.31	298-1,500	0.315	22	15, 646
Styrene, C <sub>6</sub> H <sub>5</sub> CH=CH <sub>2</sub>	-7.22	150.0	-99.9	25.2	29.17	298-1,500	0.134	26	15, 611, 637

Correlation constants: heat capacity of ideal gas (continued)

Table 22-1

Compound	$C_p^o = A + BT + CT^2 + DT^3$				$C_p^o$ at 298 K, cal/(g-mol)(°K)	Range, °K	Average error, %	Data points, no.	References
	A	$B \times 10^3$	$C \times 10^6$	$D \times 10^9$					
<b>Diolefins</b>									
1,3 Butadiene, $C_4H_6$	-0.56	81.1	-53.5	13.6	19.21	298-1,500	0.434	34	15,417,636
Isoprene, $C_5H_8$	0.63	100.5	-64.0	15.8	25.31	298-1,500	0.395	34	15,417,636
Chloroprene, $C_4H_5Cl$	2.93	75.6	-48.3	11.8	21.5			est.	
<b>Organic oxides</b>									
Ethylene oxide, $C_2H_4O$	-2.06	54.4	-32.1	7.31	11.53	298-1,500	0.182	28	7,15,637
Propylene oxide, $C_3H_6O$	-3.57	86.4	-61.6	18.5	17.20	298-1,000	0.314	24	15,649,654
Butylene oxide, $C_4H_8O$	-2.81	97.9	-48.6	6.1	22.2			est.	
<b>Primary alcohols</b>									
Methanol, $CH_3OH$	3.62	24.9	-7.05		10.49	298-1,000	0.429	35	15,416,418,637,692
Ethanol, $C_2H_5OH$	0.239	62.3	-38.06	9.47	15.64	298-1,500	1.357	33	15,418,637,692
<i>n</i> -Propanol, $C_3H_7OH$	2.71	68.6	-27.0	1.51	20.82	298-1,000	0.137	28	15,416,418,692
<i>n</i> -Butanol, $C_4H_9OH$	2.51	91.1	-39.6	4.09	26.29	298-1,000	0.131	26	15,418,692
<b>Chloromethanes</b>									
Methyl chloride, $CH_3Cl$	2.96	26.2	-12.6	2.35	9.74	298-1,500	0.127	49	7,15,418,727
Methylene chloride, $CH_2Cl_2$	4.3	32.7	-21.6	5.4	12.13	298-1,500	0.274	49	7,15,418,727
Chloroform, $CHCl_3$	7.71	34.3	-26.4	7.29	15.78	298-1,500	0.394	34	15,418,727
Carbon tetrachloride, $CCl_4$	12.6	33.2	-29.3	8.58	20.12	298-1,500	0.618	34	15,418,727



methane ( $CH_4$ ) as a low-pressure gas at 25 C (298.16 K).

We obtain the correlation constants ( $A$ ,  $B$ ,  $C$ ,  $D$ ) for methane from Table 22-I and substitute them into Eq. (22-1) at a temperature of 298.16 K to get:

$$C_p^o = 5.04 + 9.3 \times 10^{-3}(298.16) + 8.87 \times 10^{-6}(298.16)^2 - 5.4 \times 10^{-9}(298.16)^3$$

$$C_p^o = 8.46 \text{ cal/(g-mol)(°K)}$$

The calculated and data values compare favorably (8.46 vs. 8.53).

**Example 22-2**—Let us now calculate the energy required to heat chlorine ( $Cl_2$ ) from 25 C to 225 C at low pressure.

From thermodynamics, we recall that the change in enthalpy,  $\Delta H$ , at constant pressure is:

$$\Delta H = \int_{T_1}^{T_2} C_p^o dT$$

$$\Delta H = \int_{T_1}^{T_2} (A + BT + CT^2 + DT^3) dT$$

$$\Delta H = \left[ AT + \frac{B}{2}T^2 + \frac{C}{3}T^3 + \frac{D}{4}T^4 \right]_{T_1}^{T_2}$$

By substituting the correlation constants ( $A$ ,  $B$ ,  $C$ ,  $D$ ) for chlorine from Table 22-I and the temperature limits, ( $T_2 = 498.16$  K) and ( $T_1 = 298.16$  K) into the equation, we obtain:

$$\begin{aligned} \Delta H = & 7.00[498.16 - 298.16] + \\ & \frac{5.05 \times 10^{-2}}{2}[(498.16)^2 - (298.16)^2] - \\ & \frac{4.39 \times 10^{-9}}{3}[(498.16)^3 - (298.16)^3] + \\ & \frac{1.30 \times 10^{-9}}{4}[(498.16)^4 - (298.16)^4] \end{aligned}$$

$$\Delta H = 1,667.5 \text{ cal/g-mol}$$

## HEATS OF FORMATION

L. David Hood and Carl L. Yaws

Heats of formation for individual chemicals in chemical reactions are required to determine the heat of reaction,  $\Delta H_r^o$ , and associated heating and cooling requirements. If  $\Delta H_r^o < 0$ , then the chemical reaction is

exothermic and cooling is needed. If  $\Delta H_r^o > 0$ , the reaction is endothermic and heating is required. Agreement of calculated and data values for this procedure is very good.

Correlation constants: heat of formation of ideal gas

Table 22-11

Compound	$\Delta H_f^\circ = A + BT + CT^2$			$\Delta H_f^\circ$ at 298 K, kcal/mol	Range, °K	Average error (absolute), kcal/mol	Data points, no.	References
	A	B x 10 <sup>3</sup>	C x 10 <sup>6</sup>					
<b>Sulfur oxides</b>								
Sulfur dioxide, SO <sub>2</sub>	-69.6	-5.29	-	-70.95	298-717	0.135	14	7,15
	-86.9	0.32	-	-86.6 @ 800K	717-1,500	0.008	11	7,15
Sulfur trioxide, SO <sub>3</sub>	-93.1	-5.34	-	-94.6	298-717	0.146	14	7,15
	-110.5	0.80	-	-110.1 @ 800	717-1,500	0.199	11	7,15
<b>Nitrogen oxides</b>								
Nitrous oxide, N <sub>2</sub> O	13.1	0.803	-	19.5	298-1,500	0.114	23	7,15
Nitric oxide, NO	21.6	0.0036	-	21.6	298-1,500	0.010	23	7,15
Nitrogen dioxide, NO <sub>2</sub>	7.94	-0.178	-	8.00	298-1,500	0.097	23	7,15
<b>Carbon oxides</b>								
Carbon monoxide, CO	-26.5	0.84	-1.05	-26.4	298-1,500	0.040	23	7,15
Carbon dioxide, CO <sub>2</sub>	-93.9	-0.43	-	-94.05	298-1,500	0.019	23	7,15
<b>Hydrogen halides</b>								
Hydrogen fluoride, HF	-64.6	-0.801	-	-64.9	298-1,500	0.160	37	7,15
Hydrogen chloride, HCl	-21.9	-0.610	-	-22.06	298-1,500	0.031	37	7,15
Hydrogen bromide, HBr	-8.13	20.1	-73.4	-8.69	100-331	0.017	6	7,15
	-12.0	-1.35	0.45	-12.5 @ 400	331-1,500	0.016	19	7,15
Hydrogen iodide, HI	7.02	-2.42	-	6.3	298-386	0.011	6	7,15
	7.12	-7.67	-	4.06 @ 400	386-457	0.005	4	7,15
	-0.85	-1.24	0.45	-1.55 @ 800	457-1,500	0.005	17	7,15
<b>Nitrogen hydrides</b>								
Ammonia, NH <sub>3</sub>	-9.34	-6.20	2.36	-10.9	298-1,500	0.036	22	7,15
Hydrazine, N <sub>2</sub> H <sub>4</sub>	24.7	-8.01	4.02	22.8	298-1,500	0.124	37	7,15,218
<b>Hydrogen oxides</b>								
Water, H <sub>2</sub> O	-57.4	-1.79	-	-57.8	298-1,500	0.0822	23	7,15
Hydrogen peroxide, H <sub>2</sub> O <sub>2</sub>	-31.8	-3.04	1.19	-32.5	298-1,500	0.043	37	7,15,245
<b>Olefins</b>								
Ethylene, C <sub>2</sub> H <sub>4</sub>	14.8	-8.81	3.15	12.53	298-1,500	0.051	51	7,11,15,417,637
Propylene, C <sub>3</sub> H <sub>6</sub>	8.44	-13.8	5.31	4.86	298-1,500	0.076	37	15,417,637
1-Butene, C <sub>4</sub> H <sub>8</sub>	4.53	-17.5	7.22	-0.03	298-1,500	0.305	37	15,417,637
<b>Alkanes</b>								
Methane, CH <sub>4</sub>	-15.4	-9.59	3.50	-17.9	298-1,500	0.042	36	15,461,637
Ethane, C <sub>2</sub> H <sub>6</sub>	-16.4	-14.8	6.13	-20.1	298-1,500	0.35	48	15,461,447,637
Propane, C <sub>3</sub> H <sub>8</sub>	-20.0	-19.1	8.15	-24.9	298-1,500	0.17	49	15,447,401,637
<b>Xylenes</b>								
<i>o</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	10.5	-23.4	9.95	4.54	298-1,500	0.102	22	15,417
<i>m</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	10.4	-24.6	10.5	4.12	298-1,500	0.118	22	15,417
<i>p</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	10.7	-25.1	10.6	4.29	298-1,500	0.115	22	15,417
<b>Aromatics</b>								
Benzene, C <sub>6</sub> H <sub>6</sub>	23.7	-15.3	6.27	19.8	298-1,500	0.092	22	15,417,637
Naphthalene, C <sub>10</sub> H <sub>8</sub>	41.5	-21.1	10.1	36.1	298-1,000	0.135	18	15,502
<b>Alkyl aromatics</b>								
Toluene, C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	16.8	-19.0	7.84	11.95	298-1,500	0.166	22	15,417
Ethylbenzene, C <sub>6</sub> H <sub>5</sub> C <sub>2</sub> H <sub>5</sub>	13.1	-23.5	10.2	7.12	298-1,500	0.129	22	15,417
Cumene, C <sub>6</sub> H <sub>5</sub> CH(CH <sub>3</sub> ) <sub>2</sub>	7.80	-27.2	12.1	0.940	298-1,500	0.162	22	15,417
<b>Benzene derivatives</b>								
Chlorobenzene, C <sub>6</sub> H <sub>5</sub> Cl	15.7	-13.0	6.40	12.39	298-1,000	0.028	9	15
Aniline, C <sub>6</sub> H <sub>5</sub> NH <sub>2</sub>	25.2	-17.6	8.98	20.76	298-1,000	0.046	9	15
Phenol, C <sub>6</sub> H <sub>5</sub> OH	-19.3	-14.6	7.18	-23.0	298-1,000	0.036	9	15
<b>Cycloalkanes</b>								
Cyclopropane, C <sub>3</sub> H <sub>6</sub>	16.9	-16.7	7.90	12.74	298-1,000	0.064	18	15,637
Cyclobutane, C <sub>4</sub> H <sub>8</sub>	12.6	-24.8	12.4	6.37	298-1,000	0.042	9	15
Cyclopentane, C <sub>5</sub> H <sub>10</sub>	-11.5	-27.8	12.3	-18.47	298-1,500	0.226	50	15,531,417,637
Cyclohexane, C <sub>6</sub> H <sub>12</sub>	-21.6	-32.0	15.8	-29.43	298-1,500	0.328	37	15,417,637
<b>Olefin monomers</b>								
Isobutylene, C <sub>4</sub> H <sub>8</sub>	0.560	-17.9	7.41	-4.04	298-1,500	0.068	22	15,417
Styrene, C <sub>6</sub> H <sub>5</sub> CH=CH <sub>2</sub>	39.6	-17.2	7.32	35.22	298-1,500	0.097	22	15,417
<b>Diolefins</b>								
1,3-Butadiene, C <sub>4</sub> H <sub>6</sub>	29.0	-10.1	4.13	26.5	298-1,500	0.234	48	15,417,630,636
Isoprene, C <sub>5</sub> H <sub>8</sub>	21.8	-14.4	6.16	18.1	298-1,500	0.079	35	15,417,636
Chloroprene, C <sub>2</sub> H <sub>3</sub> Cl	27.8	-12.1	3.78	21.02	298-1,500	-	-	Estimated
<b>Organic oxides</b>								
Ethylene oxide, C <sub>2</sub> H <sub>4</sub> O	-9.29	-12.9	6.12	-12.59	298-1,000	0.022	9	15
Propylene oxide, C <sub>3</sub> H <sub>6</sub> O	-17.7	-17.3	6.40	-22.1	298-1,000	0.093	27	15,449,654
Butylene oxide, C <sub>4</sub> H <sub>8</sub> O	-22.1	-19.5	8.29	-27.4	298-1,500	-	-	Estimated

Compound	$\Delta H_f^\circ = A + BT + CT^2$			$\Delta H_f^\circ$ at 298 K, kcal/mol	Range, °K	Average error (absolute), kcal/mol	Data points, no.	References
	A	B x 10 <sup>3</sup>	C x 10 <sup>6</sup>					
<b>Primary alcohols</b>								
Methanol, CH <sub>3</sub> OH	-44.96	-11.9	4.98	-48.08	298-1,000	0.015	35	15,418,692
Ethanol C <sub>2</sub> H <sub>5</sub> OH	-51.8	-16.6	7.59	-56.12	298-1,000	0.043	27	15,418,692
n-Propanol, C <sub>3</sub> H <sub>7</sub> OH	-55.7	-22.3	10.5	-61.55	298-1,000	0.110	27	15,418,692
n-Butanol, C <sub>4</sub> H <sub>9</sub> OH	-59.8	-26.9	12.8	-65.59	298-1,000	0.0365	27	15,418,692
<b>Chloromethanes</b>								
Methyl chloride, CH <sub>3</sub> Cl	-19.9	-2.57	-	-20.2	298-1,500	0.549	51	7,15,418,727
Methylene chloride, CH <sub>2</sub> Cl <sub>2</sub>	-21.5	-5.13	2.15	-22.8	298-1,500	0.048	51	7,15,418,727
Chloroform, CHCl <sub>3</sub>	-24.7	0.0334	-	-24.5	298-1,500	0.179	37	15,418,727
Carbon tetrachloride, CCl <sub>4</sub>	-24.0	2.42	-	-23.5	298-1,500	0.358	37	15,418,727

## Correlation constants—Table 22-II

The correlation for heat of formation of the ideal gas at low pressure is based on a series expansion in temperature:

$$\Delta H_f^\circ = A + BT + CT^2 \quad (22-2)$$

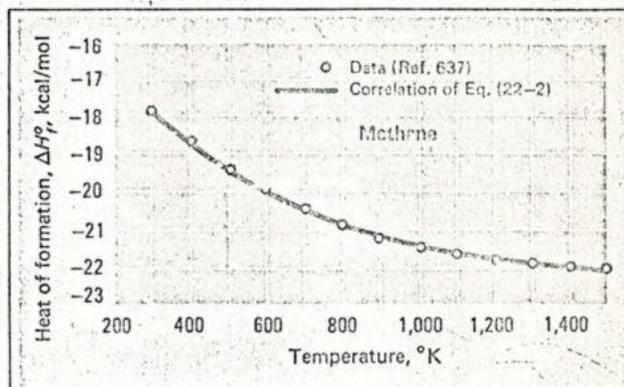
where  $\Delta H_f^\circ$  = heat of formation of ideal gas at low pressure, kcal/g-mol;  $A$ ,  $B$ ,  $C$  = correlation constants characteristic for the chemical compound; and  $T$  = temperature, °K.

A least squares regression analysis of the available data was used to determine the constants  $A$ ,  $B$  and  $C$ . A generalized least-squares regression computer program for minimizing deviation was used to process the numerous data points.

Correlation and data values are compared in Fig. 22-2 for a representative chemical compound. The agreement is quite good. In most cases, the average absolute deviations of correlation and data are less than 0.2 kcal/g-mol.

*Example 22-3*—Let us estimate the heat of formation of ethylene (C<sub>2</sub>H<sub>4</sub>) as an ideal gas at 400 K.

Substituting the values of the correlation constants  $A$ ,  $B$  and  $C$  for ethylene from Table 22-II and tempera-



Heat of formation

Fig. 2

ture  $T = 400$  K into Eq. 22-2 yields:

$$\Delta H_f^\circ = 14.8 + (-8.81 \times 10^{-3})(400) + 3.15 \times 10^{-6}(400)^2$$

$$\Delta H_f^\circ = 11.78 \text{ kcal/g-mol}$$

The calculated value compares favorably with the data results (11.78 vs. 11.79).

## FREE ENERGIES OF FORMATION

Cecil E. Gorin II and Carl L. Yaws

Gibbs free energy of formation is important in chemical-reaction engineering. (Two notations are used to denote Gibbs free energy of formation:  $\Delta F_f^\circ$  and  $\Delta G_f^\circ$ . Usage of  $\Delta G_f^\circ$  is increasing and is adopted here.) Values for the free energy of formation for individual chemicals are required to determine the free energy of reaction,  $\Delta G_r^\circ$ , and the accompanying chemical thermodynamic equilibrium for the reaction.

In addition, the following criteria are generally true for screening the feasibility of chemical reactions:

Reaction promising:

$$\Delta G_r^\circ < 0 \text{ kcal/g-mol}$$

Reaction possibly promising:

$$0 < \Delta G_r^\circ < 10 \text{ kcal/g-mol}$$

Reaction not promising:

$$\Delta G_r^\circ > 10 \text{ kcal/g-mol}$$

## Correlation constants—Table 22-III

Correlation constants for Gibbs free energy of formation of the ideal gas at low pressure were based on a linear relationship in temperature:

$$\Delta G_f^\circ = A + BT \quad (22-3)$$

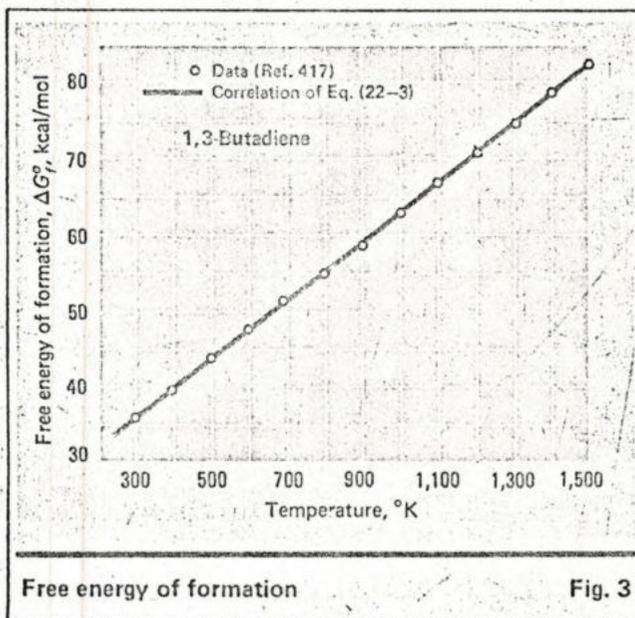
where  $\Delta G_f^\circ$  = free energy of formation of ideal gas at

Correlation constants: free energy of formation of ideal gas

Table 22-III

Compound	$\Delta G_f^\circ = A + BT$		$\Delta G_f^\circ$ at 298 K, kcal/mol	Range, °K	Average error (absolute), kcal/mol	Data points, no.	References
	A	B x 10 <sup>3</sup>					
<b>Sulfur oxides</b>							
Sulfur dioxide, SO <sub>2</sub>	-71.9	0.25	-71.7	298-717	0.107	13	7,15
	-86.8	17.7	-72.6 @ 800	717-1,500	0.193	12	7,15
Sulfur trioxide, SO <sub>3</sub>	-95.6	23.1	-88.6	298-717	0.118	13	7,15
	-110.	39.7	-78.2 @ 800	717-1,500	0.104	12	7,15
<b>Nitrogen oxides</b>							
Nitrous oxide, N <sub>2</sub> O	19.6	17.7	24.9	298-1,500	0.065	23	7,15
Nitric oxide, NO	21.6	-3.02	20.7	298-1,500	0.008	23	7,15
Nitrogen dioxide, NO <sub>2</sub>	7.82	15.1	12.3	298-1,500	0.069	23	7,15
<b>Carbon oxides</b>							
Carbon monoxide, CO	-26.5	-21.3	-32.8	298-1,500	0.074	23	7,15
Carbon dioxide, CO <sub>2</sub>	-94.2	-0.42	-94.3	298-1,500	0.029	23	7,15
<b>Hydrogen halides</b>							
Hydrogen fluoride, HF	-65.2	-1.25	-65.5	298-1,500	0.151	23	7,15
Hydrogen chloride, HCl	-22.3	-1.72	-22.8	298-1,500	0.047	23	7,15
Hydrogen bromide, HBr	-5.02	-25.9	-12.8	298-331	0.023	5	7,15
	-12.7	-1.76	-13.4 @ 400	331-1,500	0.036	20	7,15
Hydrogen iodide, HI	5.72	-17.9	0.38	298-586	0.001	5	7,15
	2.05	-9.04	-1.53 @ 400	386-457	0.035	4	7,15
	-1.56	-1.78	-2.41 @ 500	457-1,500	0.014	18	7,15
<b>Nitrogen hydrides</b>							
Ammonia, NH <sub>3</sub>	-12.3	27.2	-3.89	298-1,500	0.178	23	7,15
Hydrazine, N <sub>2</sub> H <sub>4</sub>	21.3	54.9	38.0	298-1,500	0.223	37	7,15,218
<b>Hydrogen oxides</b>							
Water, H <sub>2</sub> O	-58.6	12.7	-54.6	298-1,500	0.138	23	7,15
Hydrogen peroxide, H <sub>2</sub> O <sub>2</sub>	-33.2	26.4	-25.2	298-1,500	0.101	37	7,15,245
<b>Olefins</b>							
Ethylene, C <sub>2</sub> H <sub>4</sub>	10.4	18.1	16.3	298-1,500	0.291	51	7,11,15,417,637
Propylene, C <sub>3</sub> H <sub>6</sub>	1.80	41.9	15.0	298-1,500	0.401	37	15,417,637
1-Butene, C <sub>4</sub> H <sub>8</sub>	-3.43	66.5	17.1	298-1,500	0.414	37	15,417,637
<b>Alkanes</b>							
Methane, CH <sub>4</sub>	-20.1	24.9	-12.2	298-1,500	0.298	37	15,461,637
Ethane, C <sub>2</sub> H <sub>6</sub>	-23.3	49.7	-7.83	298-1,500	0.388	51	15,447,461,637
Propane, C <sub>3</sub> H <sub>8</sub>	-28.8	74.7	-5.68	298-1,500	0.467	51	15,447,461,637
<b>Xylenes</b>							
<i>o</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-0.12	94.9	29.2	298-1,500	0.565	23	15,417
<i>m</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-0.79	94.4	28.4	298-1,500	0.609	23	15,417
<i>p</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	-0.74	95.9	29.0	298-1,500	0.630	23	15,417
<b>Aromatics</b>							
Benzene, C <sub>6</sub> H <sub>6</sub>	16.7	45.9	31.0	298-1,500	0.409	38	15,417,637
Naphthalene, C <sub>10</sub> H <sub>8</sub>	33.3	66.4	53.5	298-1,000	0.327	18	15,502
<b>Alkyl aromatics</b>							
Toluene, C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	7.80	68.7	29.2	298-1,500	0.557	23	15,417
Ethylbenzene, C <sub>6</sub> H <sub>5</sub> C <sub>2</sub> H <sub>5</sub>	2.67	93.0	31.2	298-1,500	0.648	23	15,417
Cumene, C <sub>6</sub> H <sub>5</sub> CH(CH <sub>3</sub> ) <sub>2</sub>	-4.32	121.	32.7	298-1,500	0.619	23	15,417
<b>Benzene derivatives</b>							
Chlorobenzene, C <sub>6</sub> H <sub>5</sub> Cl	10.7	42.9	23.7	298-1,000	0.192	9	15
Aniline, C <sub>6</sub> H <sub>5</sub> NH <sub>2</sub>	18.5	70.6	39.8	298-1,000	0.248	9	15
Phenol, C <sub>6</sub> H <sub>5</sub> OH	-25.0	56.5	-7.86	298-1,000	0.219	9	15
<b>Cycloalkanes</b>							
Cyclopropane, C <sub>3</sub> H <sub>6</sub>	10.3	47.7	24.9	298-1,000	0.260	14	15,637
Cyclobutane, C <sub>4</sub> H <sub>8</sub>	3.09	76.2	26.3	298-1,000	0.366	9	15
Cyclopentane, C <sub>5</sub> H <sub>10</sub>	-24.1	108.	9.23	298-1,500	0.617	51	15,591,417,637
Cyclohexane, C <sub>6</sub> H <sub>12</sub>	-35.1	139.	7.59	298-1,500	0.532	37	15,417,637
<b>Olefin monomers</b>							
Isobutylene, C <sub>4</sub> H <sub>8</sub>	-7.68	69.6	13.9	298-1,500	0.465	23	15,417
Styrene, C <sub>6</sub> H <sub>5</sub> CH=CH <sub>2</sub>	32.0	62.4	51.1	298-1,500	0.729	22	15,417
<b>Diolefins</b>							
1,3-Butadiene, C <sub>4</sub> H <sub>6</sub>	24.2	38.6	36.2	298-1,500	0.325	51	15,417,637,636
Isoprene, C <sub>5</sub> H <sub>8</sub>	15.2	63.8	34.9	298-1,500	0.348	23	15,417,636
Chloroprene, C <sub>4</sub> H <sub>5</sub> Cl	19.1	39.6	31.1	298-1,500	0.488	4	Estimated
<b>Organic oxides</b>							
Ethylene oxide, C <sub>2</sub> H <sub>4</sub> O	-14.4	36.8	-3.13	298-1,000	0.203	9	15
Propylene oxide, C <sub>3</sub> H <sub>6</sub> O	-24.5	60.4	-6.17	298-1,000	0.267	10	15,634
Butylene oxide, C <sub>4</sub> H <sub>8</sub> O	-31.6	88.5	-4.92	298-1,500	0.255	4	Estimated

Compound	$\Delta G_f^\circ = A + BT$		$\Delta G_f^\circ$ at 298 K, kcal/mol	Range, °K	Average error (absolute), kcal/mol	Data points, no.	References
	A	B x 10 <sup>3</sup>					
<b>Primary alcohols</b>							
Methanol, CH <sub>3</sub> OH	-50.2	36.5	-38.8	298-1,000	0.292	35	15,418,637,692
Ethanol, C <sub>2</sub> H <sub>5</sub> OH	-58.3	59.7	-40.1	298-1,000	0.341	27	15,418,692
<i>n</i> -Propanol, C <sub>3</sub> H <sub>7</sub> OH	-64.5	84.8	-38.8	298-1,000	0.368	27	15,418,692
<i>n</i> -Butanol, C <sub>4</sub> H <sub>9</sub> OH	-69.4	110.	-36.0	298-1,000	0.420	27	15,418,692
<b>Chloromethanes</b>							
Methyl chloride, CH <sub>3</sub> Cl	-22.0	23.7	-14.5	298-1,500	0.545	51	7,15,418,727
Methylene chloride, CH <sub>2</sub> Cl <sub>2</sub>	-23.9	24.2	-16.5	298-1,500	0.132	51	7,15,418,727
Chloroform, CHCl <sub>3</sub>	-24.8	26.9	-16.7	298-1,500	0.158	37	15,418,727
Carbon tetrachloride, CCl <sub>4</sub>	-22.6	32.1	-12.8	298-1,500	0.422	37	15,418,727



low pressure, kcal/g-mol;  $A$ ,  $B$  = correlation constants characteristic of the chemical compound; and  $T$  = temperature, °K.

The correlation constants,  $A$  and  $B$ , were ascertained from a least-squares regression analysis of the available data. The regression analysis was done with a generalized least-squares computer program for minimizing deviation.

Correlation and data values for free energy of formation compare favorably, as illustrated in Fig. 22-3 for a representative chemical.

Average absolute deviations between correlation and data values are less than 0.6 kcal/g-mol in most cases.

*Example 22-4*—Let us now estimate the free energy of formation of methanol (CH<sub>3</sub>OH) as an ideal gas at 400 K.

Substituting values for the correlation constants,  $A$  and  $B$ , for methanol from Table 22-III, and the temperature of 400 K into Eq. (22-3), yields:

$$\Delta G_f^\circ = -20.1 + 0.0249(400)$$

$$\Delta G_f^\circ = -10.14 \text{ kcal/g-mol}$$

## HEATS OF VAPORIZATION

Shailesh B. Thakore, Joseph W. Miller, Jr. and Carl L. Yaws

Heat-of-vaporization data are important in process engineering design. In distillation, heat-of-vaporization values are needed to determine the heat requirements for the reboiler. Such values are also needed to establish cooling requirements for the condenser handling the overhead fraction from the distillation. Additional usage includes process-energy requirements for unit operations involving saturated-liquid and vapor phases.

### Correlation constants—Table 22-IV

Heats of vaporization at any temperature are based on the original Watson correlation:

$$\Delta H_v = \Delta H_{v1} \left[ \frac{T_c - T}{T_c - T_1} \right]^n \quad (22-4)$$

where  $\Delta H_v$  = heat of vaporization at any temperature, cal/g;  $\Delta H_{v1}$  = heat of vaporization at  $T_1$ , cal/g;  $T_c$  = critical temperature, °K;  $T$  = temperature, °K;  $T_1$  = temperature for  $\Delta H_{v1}$ , °K; and  $n$  = characteristic constant for the chemical (in most cases,  $n = 0.38$ ).

Values for the correlation constants ( $\Delta H_{v1}$ ,  $T_1$  and  $n$ ) are given in Table 22-IV. Results for  $\Delta H_{v1}$  at  $T_1$  are based on extensive screening of the literature and selection of recommended values from the experimental investigations. The temperature range over which the correlation constants are usable is also given. In most cases, the usable range covers the entire saturated-liquid state, from the melting point to the critical point.

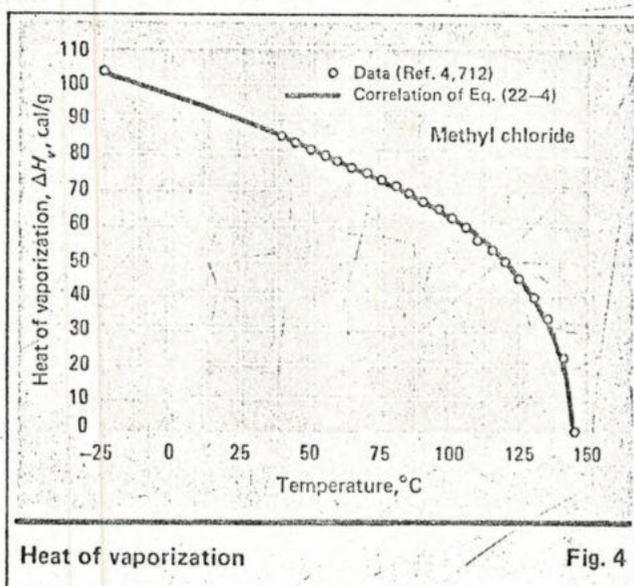
Calculated and data values are compared in Fig. 22-4 for a representative chemical. The average devi-

Correlation constants: heat of vaporization

Table 22-IV

Compound	$\Delta H_{v1}$ , cal/g	$T_1$ , °C	$T_c$ , °C	$n$	Range, °C	References	$\Delta H_v = \Delta H_{v1} \left[ \frac{T_c - T}{T_c - T_1} \right]^n$
<b>Halogens</b>							
Fluorine, F <sub>2</sub>	41.1	-188.1	-129.0	0.38	-219.6 to -129.0	1,4,9,10,14,43,70	
Chlorine, Cl <sub>2</sub>	69.6	-34.06	144.0	0.38	-101.0 to 144.0	1,9,14,30,43,70	
Bromine, Br <sub>2</sub>	44.8	58.78	315.0	0.38	-7.2 to 315.0	1,4,9,14,43,70	
Iodine, I <sub>2</sub>	39.3	184.4	546.0	0.38	112.6 to 546.0	1,4,9,43,62,70	
<b>Sulfur oxides</b>							
Sulfur dioxide, SO <sub>2</sub>	93.0	-10.0	157.6	0.38	-72.7 to 157.6	10,12,13,73,81,90	
Sulfur trioxide, SO <sub>3</sub>	128.0	44.8	218.3	0.38	16.8 to 218.3	13,85,91	
<b>Nitrogen oxides</b>							
Nitrous oxide, N <sub>2</sub> O	89.9	-89.5	36.5	0.38	-90.8 to 36.5	1,9,10,12,14,118	
Nitric oxide, NO	110.0	-151.8	-93.1	0.38	-163.8 to -93.1	1,9,10,12,14	
Nitrogen dioxide, NO <sub>2</sub>	99.0	21.2	158.0	0.38	-11.2 to 158.0	1,10,4,14	
<b>Carbon oxides</b>							
Carbon monoxide, CO	51.6	-191.5	-140.1	0.38	-205.0 to -140.1	9,10,13,14,115	
Carbon dioxide, CO <sub>2</sub>	56.1	0	31.1	0.38	-56.5 to 31.1	9,10,13,14,115,157	
<b>Hydrogen halides</b>							
Hydrogen fluoride, HF		(Equation not valid for HF)				4,10,183,184,185	
Hydrogen chloride, HCl	105.8	-85.03	51.5	0.38	-114.2 to 51.5	1,4,6,10,12,30,167,174	
Hydrogen bromide, HBr	52.0	-66.8	90.0	0.38	-86.9 to 90.0	4,6,10,12,167	
Hydrogen iodide, HI	36.9	-35.5	151.0	0.38	-50.8 to 151.0	1,6,10,12,167,174	
<b>Nitrogen hydrides</b>							
Ammonia, NH <sub>3</sub>	327.4	-33.43	132.4	0.38	-77.74 to 132.4	2,6,9,10,13,14,194	
Hydrazine, N <sub>2</sub> H <sub>4</sub>	302	113.5	380	0.38	2.0 to 380	14,189,195,206,218	
<b>Hydrogen oxides</b>							
Water, H <sub>2</sub> O	538.7	100	374.2	0.38	0 to 374.2	9,12,239,246	
Hydrogen peroxide, H <sub>2</sub> O <sub>2</sub>	321.9	150.2	455	0.38	-0.43 to 455	4,210,242,256,257,260	
<b>Diatomic gases</b>							
Hydrogen, H <sub>2</sub>	107	-252.8	-240.2	0.237	-259.4 to -240.2	10,284,293,302,306,307,309,335	
Nitrogen, N <sub>2</sub>	47.5	-195.8	-146.8	0.38	-209.9 to -146.8	10,43,45,47,277,300,306,317	
Oxygen, O <sub>2</sub>	50.9	-183.0	-119.5	0.38	-218.4 to -119.5	10,43,45,47,296,300,306,309,317	
<b>Inert gases</b>							
Helium, He	5.2	-268.9	-268.0	0.38	-269.9 to -268.0	10,43,311,322,345,387	
Neon, Ne	20.52	-246.0	-228.7	0.38	-248.7 to -228.7	10,43,47,345	
Argon, Ar	38.99	-185.9	-122.4	0.38	-189.3 to -122.4	10,43,47,345	
<b>Olefins</b>							
Ethylene, C <sub>2</sub> H <sub>4</sub>	115.4	-103.7	9.9	0.38	-169.2 to 9.9	3,10,246,414,415,419,440	
Propylene, C <sub>3</sub> H <sub>6</sub>	104.6	-47.7	91.9	0.38	-185.3 to 91.9	3,10,246,414,415,419,440	
1-Butene, C <sub>4</sub> H <sub>8</sub>	93.4	-6.3	146.2	0.38	-185.4 to 146.2	3,10,246,414,415,419	
<b>Alkenes</b>							
Methane, CH <sub>4</sub>	121.7	-161.5	-82.6	0.38	-182.6 to -82.6	3,10,47,246,417,419,454	
Ethane, C <sub>2</sub> H <sub>6</sub>	116.7	-89.2	32.3	0.38	-163.2 to 32.3	3,10,246,417,419,453	
Propane, C <sub>3</sub> H <sub>8</sub>	101.8	-42.1	96.7	0.38	-187.7 to 96.7	3,10,246,417,419,453	
<b>Xylenes</b>							
<i>o</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	82.9	144.4	357.8	0.38	-25.2 to 357.8	2,4,9,417,419,484	
<i>m</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	81.9	139.1	343.8	0.38	-47.9 to 343.8	2,4,9,417,419,484	
<i>p</i> -Xylene, C <sub>6</sub> H <sub>4</sub> (CH <sub>3</sub> ) <sub>2</sub>	81.0	138.4	344.0	0.38	13.3 to 344.0	2,4,9,417,419,472,484	
<b>Aromatics</b>							
Benzene, C <sub>6</sub> H <sub>6</sub>	94.1	80.10	288.94	0.38	5.53 to 288.94	3,4,15,309,415,417,419	
Naphthalene, C <sub>10</sub> H <sub>8</sub>	80.7	218.00	475.02	0.38	80.55 to 475.02	3,6,419	
<b>Alkyl aromatics</b>							
Toluene, C <sub>6</sub> H <sub>5</sub> CH <sub>3</sub>	86.1	110.6	318.8	0.38	-95.0 to 318.8	4,413,415,417,419,516	
Ethylbenzene, C <sub>6</sub> H <sub>5</sub> C <sub>2</sub> H <sub>5</sub>	80.0	136.2	344	0.38	-95.0 to 344	413,415,417,419,516	
Cumene, C <sub>6</sub> H <sub>5</sub> CH(CH <sub>3</sub> ) <sub>2</sub>	74.6	152.4	350	0.38	-96.0 to 350	4,413,415,417,419,516	
<b>Benzene derivatives</b>							
Chlorobenzene, C <sub>6</sub> H <sub>5</sub> Cl	76.0	131.7	359.2	0.38	-45.2 to 359.2	3,4,413,574	
Aniline, C <sub>6</sub> H <sub>5</sub> NH <sub>2</sub>	112.4	184.4	426.0	0.38	-6.15 to 426.0	3,4,413,574	
Phenol, C <sub>6</sub> H <sub>5</sub> OH	116.1	181.8	420.0	0.38	40.75 to 420.0	3,547,563	
<b>Cycloalkanes</b>							
Cyclopropane, C <sub>3</sub> H <sub>6</sub>	113.8	-32.80	124.9	0.33	-127.42 to 124.9	15,417,609,605	
Cyclobutane, C <sub>4</sub> H <sub>8</sub>	103.0	12.51	190.4	0.38	-90.73 to 190.4	15,417,604	
Cyclopentane, C <sub>5</sub> H <sub>10</sub>	93.0	49.26	238.5	0.38	-93.83 to 238.5	15,413,417,419,591	
Cyclohexane, C <sub>6</sub> H <sub>12</sub>	85.1	80.74	260.3	0.38	6.55 to 260.3	15,413,417,419,577,582	
<b>Olefin monomers</b>							
Isobutylene, C <sub>4</sub> H <sub>8</sub>	84.22	-6.9	144.7	0.38	-140.35 to 144.7	3,10,417,607,611,619,620	
Styrene, C <sub>6</sub> H <sub>5</sub> CH=CH <sub>2</sub>	84.69	145.0	369.0	0.33	-30.6 to 369.0	3,611,623,622	
<b>Diolenes</b>							
1,3-Butadiene, C <sub>4</sub> H <sub>6</sub>	100.2	-4.41	152.0	0.33	-106.9 to 152.0	10,419,620,609,640	
Isoprene, C <sub>5</sub> H <sub>8</sub>	91.5	34.67	210.2	0.38	-146.0 to 210.2	419,620	
Chloroprene, C <sub>4</sub> H <sub>6</sub> Cl	72.3	60.0	261.7	0.38	-101.0 to 261.7	4,620	

Compound	$\Delta H_{v1}$ , cal/g	$T_1$ , °C	$T_c$ , °C	$n$	Range, °C	References	$\Delta H_v = \Delta H_{v1} \left[ \frac{T_c - T}{T_c - T_1} \right]^n$
<b>Organic oxides</b>							
Ethylene oxide, C <sub>2</sub> H <sub>4</sub> O	138.5	10.55	195.8	0.466	-112.5 to 195.8	4,10,15,309,574,657,658,659,660	
Propylene oxide, C <sub>3</sub> H <sub>6</sub> O	114.8	25.0	209.1	0.466	-112.0 to 209.1	4,656,657,658	
Butylene oxide, C <sub>4</sub> H <sub>8</sub> O	100.5	63.2	252.6	0.466	-150.0 to 252.6	4,657	
<b>Primary alcohols</b>							
Methanol, CH <sub>3</sub> OH	260.1	64.7*	239.4	0.40	-97.6 to 239.4	4,9,15,413,646,692	
Ethanol, C <sub>2</sub> H <sub>5</sub> OH	202.6	78.3*	243.1	0.40	-114.1 to 243.1	4,9,15,413,646,692	
n-Propanol, C <sub>3</sub> H <sub>7</sub> OH	162.3	97.2*	263.6	0.40	-126.2 to 263.6	4,9,15,413,646,670,672,678,691,692	
n-Butanol, C <sub>4</sub> H <sub>9</sub> OH	140.5	117.7*	289.6	0.40	-89.3 to 289.8	4,9,15,413,646,692	
<b>Chloromethanes</b>							
Methyl chloride, CH <sub>3</sub> Cl	102.2	-23.8	143.1	0.38	-97.7 to 143.1	4,9,15,574,708,712,718,725	
Methylene chloride, CH <sub>2</sub> Cl <sub>2</sub>	78.7	39.8	241.0	0.38	-96.7 to 241.0	4,9,15,574,708,718,721	
Chloroform, CHCl <sub>3</sub>	58.9	61.3	263.4	0.38	-63.2 to 263.4	4,9,15,574,708,718,721	
Carbon tetrachloride, CCl <sub>4</sub>	46.55	76.7	283.2	0.38	-22.9 to 283.2	4,9,15,574,708,718,721	



ations between correlation and data values are in most cases less than 1 to 5%.

**Example 22-5**—Let us estimate the heat of vaporization of methyl chloride (CH<sub>3</sub>Cl) at 40°C.

From Table 22-IV, we obtain the correlation constants for methyl chloride as:

$$\begin{aligned} T &= 40 \text{ C} = 313.2 \text{ K} \\ T_c &= 143.1 \text{ C} = 416.3 \text{ K} \\ T_1 &= -23.8 \text{ C} = 249.4 \text{ K} \\ \Delta H_{v1} &= 102.2 \text{ cal/g} \end{aligned}$$

By substituting these values into Eq. (22-4); we obtain:

$$\Delta H_v = 102.2 \left[ \frac{416.3 - 313.2}{416.3 - 249.4} \right]^{0.38}$$

$$\Delta H_v = 85.10 \text{ cal/g}$$

The calculated and data values compare favorably (85.10 vs. 83.84).

## References

The reference citations listed in this article appeared in Parts 1 through 21 of this series. References 1-72. Part 1, June 10, 1974, p. 78; 73-93, Part 2, July 8, 1974, p. 92; 94-134, Part 3, Aug. 19, 1974, p. 106; 135-157, Part 4, Sept. 30, 1974, p. 122; 158-187, Part 5, Oct. 28, 1974, p. 122; 188-235, Part 6, Nov. 25, 1974, p. 100; 236-262, Part 7, Dec. 23, 1974, p. 74; 263-336, Part 8, Jan. 20, 1975, p. 106; 337-408, Part 9, Feb. 17, 1975, p. 94; 409-443, Part 10, Mar. 31, 1975, p. 109; 444-469, Part 11, May 12, 1975, p. 97; 470-490, Part 12, July 21, 1975, p. 122; 491-515, Part 13, Sept. 1, 1975, p. 115; 516-546, Part 14, Sept. 29, 1975, p. 81; 547-574, Part 15, Oct. 27, 1975, p. 127; 575-606, Part 16, Dec. 8, 1975, p. 128; 607-629, Part 17, Jan. 19, 1976, p. 115; 630-646, Part 18, Mar. 1, 1976, p. 115; 647-665, Part 19, Apr. 12, 1976, p. 137; 666-704, Part 20, June 7, 1976, p. 127; 705-734, Part 21, July 5, 1976, p. 89.

## The Authors

**Robin W. Borreson** is a senior in chemical engineering at Lamar University. She is active in AIChE and chairperson of the Soc. of Women Engineers. She is a member of ACS, Omega Chi Epsilon, Tau Beta Pi and Phi Kappa Phi.

**Cecil E. Gorin II** is a senior in chemical engineering at Lamar University. He has worked in process engineering with Neches Butane Products Co. as part of the cooperative education program. He is a member of Tau Beta Pi, Omega Chi Epsilon and Phi Kappa Phi, and is a student member of AIChE.

**L. David Hood** is working toward a degree in chemical engineering at Lamar University. He was formerly employed as a process engineer by Texas Instruments Co. He has a B.S. in chemistry from Lamar University and is president of the AIChE student chapter there.

**Joseph W. Miller, Jr.** is assistant professor of chemical engineering at Lamar University. He holds the B.Ch.E., M. Eng., M.S., Ch.E. and Ph.D. from the University of Louisville. He is a member of AIChE and Sigma Xi. His chief interests are in mass transfer and transport phenomena.

**Gordon R. Schorr** is a process engineer at Goodyear Chemical Div., Beaumont, Tex., where he has worked on isoprene, polyisoprene and polybutadiene processes. He has a B.Ch.E. from Rensselaer Polytechnic Institute and an M.E. in chemical engineering from Lamar University. He is a member of AIChE.

**Shailesh B. Thakore** received an M.E. in chemical engineering from Lamar University this year. He has a B.S. in chemical engineering from Louisiana State University and obtained a B.S. in chemistry in India. He is a member of AIChE.

**Carl L. Yaws** is associate professor in the Chemical Engineering Dept. of Lamar University, P. O. Box 10053, Beaumont, TX 77710. His industrial experience has been primarily in research and development and design with Exxon Corp., Ethyl Corp. and Texas Instruments Co. He received a B.S. in chemical engineering from Texas A&I University, and an M.S. and Ph.D. in chemical engineering from the University of Houston. He has written more than 25 technical articles on mass transfer, distillation, reaction kinetics, process scaleup and property data.